



# DESIGN OF ACTIVE STRUCTURED REACTOR FOR BIOGAS EXHAUST ABATEMENT

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# BIOGAS - VALUABLE ALTERNATIVE FUEL



## Potential sources<sup>1</sup>:

- ▶ agricultural residues
- ▶ animal waste
- ▶ food and kitchen organic waste
- ▶ forestry crops and residues
- ▶ waste water sludge
- ▶ landfill gas
- ▶ municipal organic waste
- ▶ industrial residues

## Composition<sup>2,3</sup>

- ▶ CH<sub>4</sub> (50 - 75%)
- ▶ CO<sub>2</sub> (25 - 45%)
- ▶ H<sub>2</sub>O (2 - 7%)
- ▶ N<sub>2</sub> (< 2 %)
- ▶ O<sub>2</sub> (< 2 %)
- ▶ H<sub>2</sub> (< 1 %)
- ▶ H<sub>2</sub>S (20 - 20,000 ppm)

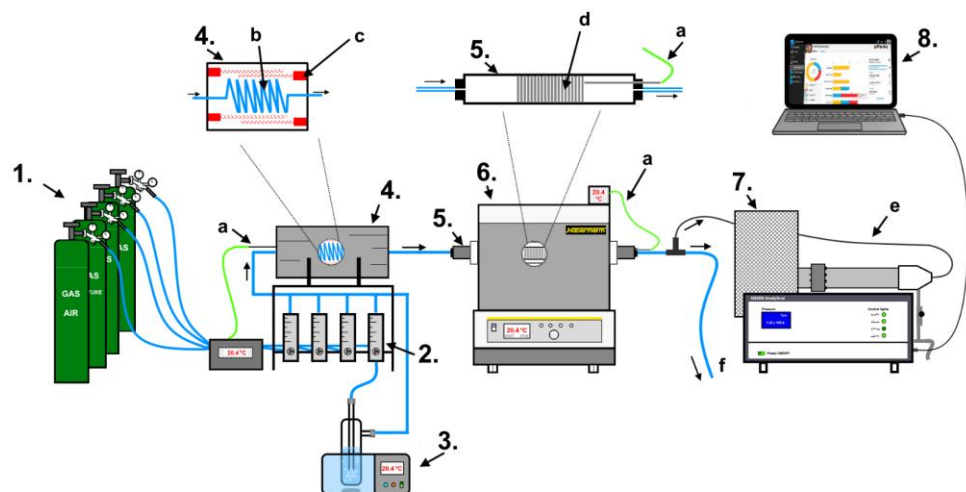
# BIOGAS - VALUABLE ALTERNATIVE FUEL



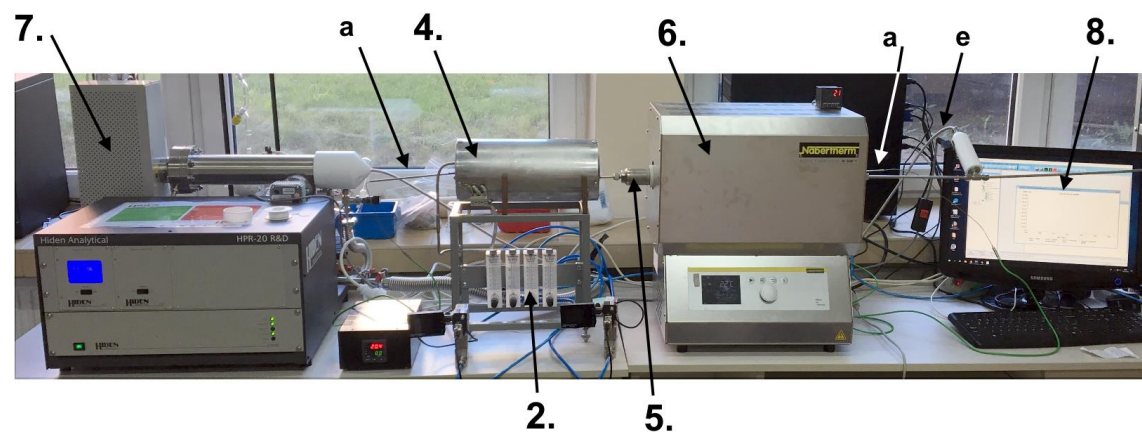
## Potential usage

- ▶ production of heat and/or steam
- ▶ domestic and industrial heating, cooling and electricity
- ▶ electricity production / combined heat and power production (CHP)
- ▶ fuel for motor vehicle
- ▶ fuel cells
- ▶ chemical manufacturing
- ▶ injection into gas grid

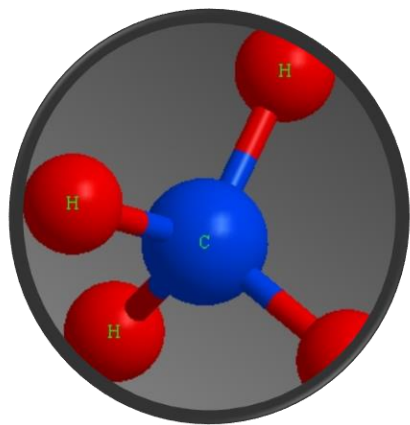
# STRUCTURED CATALYTIC CONVERTERS



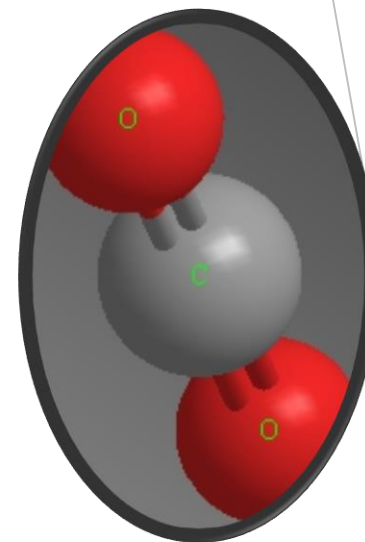
Schematic diagram and photograph of catalytic testing rig: 1 - gases cylinders, 2 - rotameters, 3 - water evaporator, 4 - pre-heater, 5 - converter, 6 - furnace, 7 - mass spectrometer, 8 - computer; a) thermocouple, b) pre-heater stainless steel coil (2 m), c) heating wire, d) wire gauzes, e) mass spectrometer capillary, f) vent.



# CATALYTIC COMBUSTION – CONDITIONS



- ▶ Temperature: 100 - 500 °C
- ▶ Flow rate: 1 - 6 dm<sup>3</sup>/min
- ▶ Catalyst: CoPd/Al<sub>2</sub>O<sub>3</sub>
- ▶ Catalyst support: stainless steel wire gauze



hydraulic diameter, [m]	specific surface area, [m <sup>2</sup> /m <sup>3</sup> ]	porosity
1.71x10 <sup>-3</sup>	1822.90	0.78

# BIOGAS COMPOSITIONS FOR EXPERIMENTS



## composition I (MIX 1)

simulate biogas engine start-up  
or shut-down

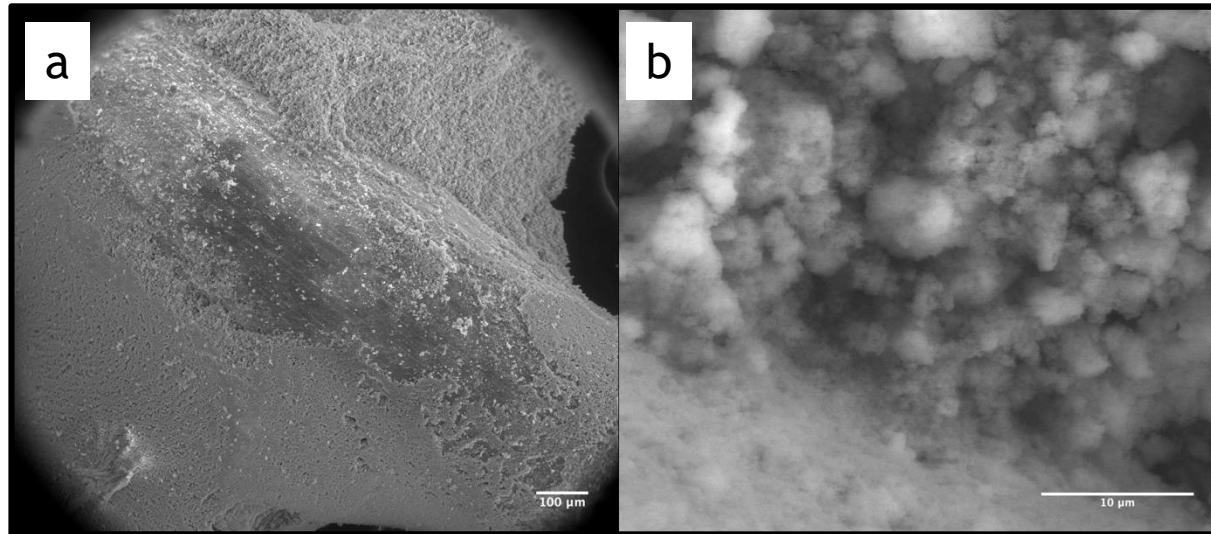
## composition II (MIX 2)

simulate dry reacting mixture

Compound	Unit	MIX 1	MIX 2
CH <sub>4</sub> ,*	vol%	0.40	0.40
O <sub>2</sub>	vol%	8.00	8.00
CO	vol%	0.05	0.05
CO <sub>2</sub>	vol%	7.00	7.00
NO	ppm	200.0	200.0
NO <sub>x</sub>	ppm	240.0	240.0
NH <sub>3</sub>	ppm	-	2500
N <sub>2</sub>		balance	balance

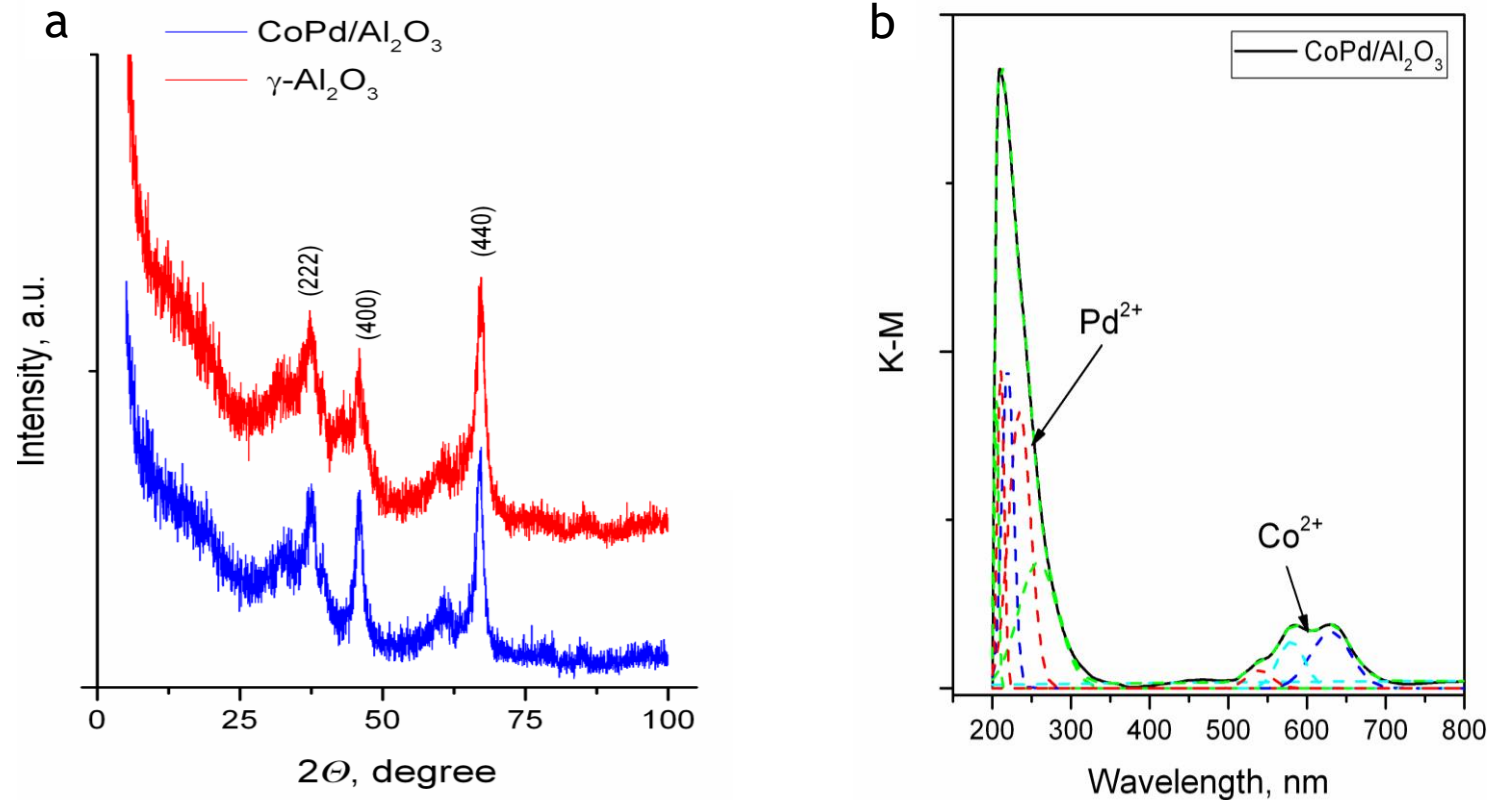


# SEM CHARACTERIZATION



SEM pictures of prepared wire gauze supported structured catalysts  
a) scale 100  $\mu\text{m}$ , b) scale 10  $\mu\text{m}$

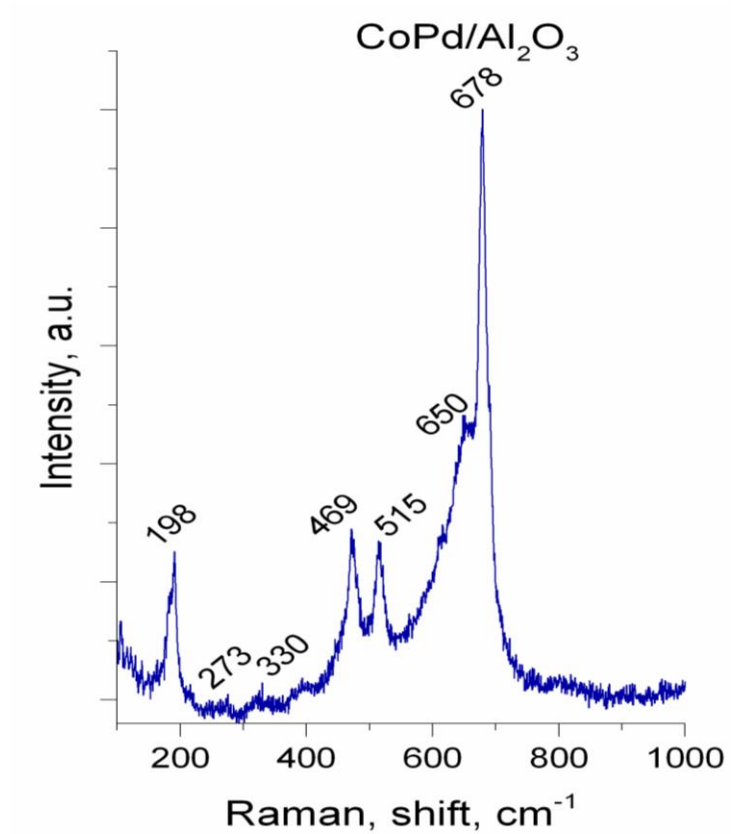
# SPECTROSCOPIC CHARACTERIZATION



Results for tested catalysts a) XRD diffractogram, b) UV-Vis spectrum

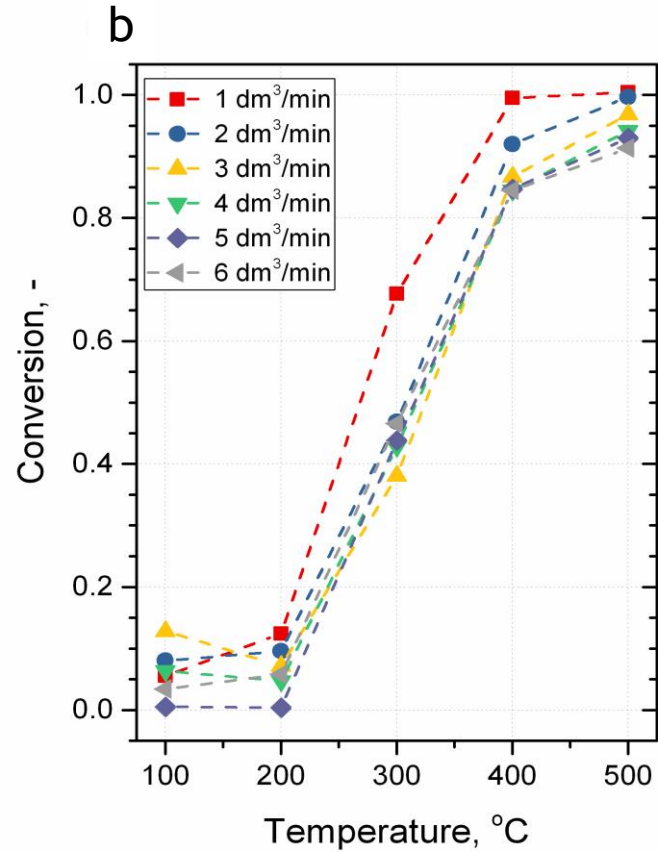
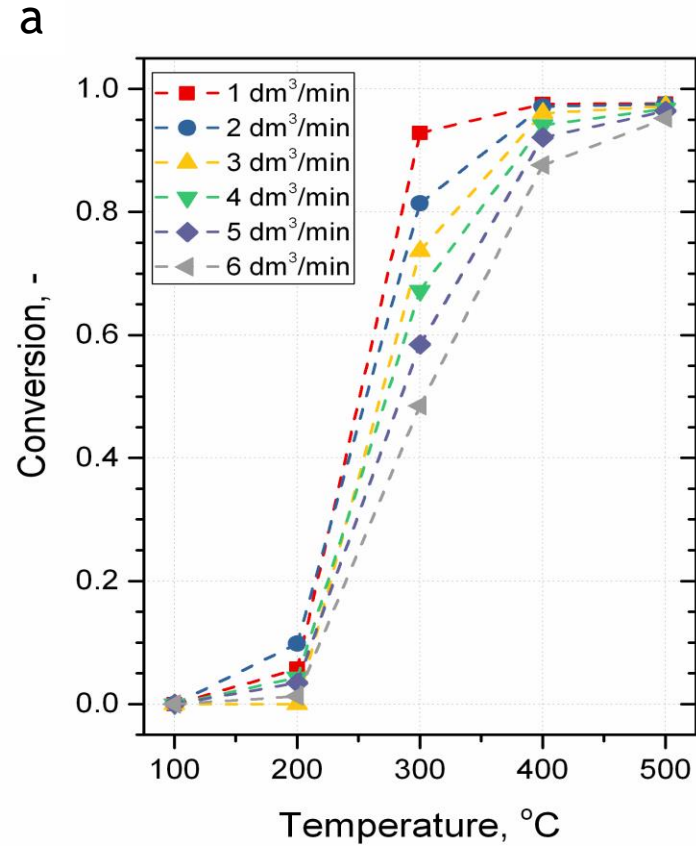


# SPECTROSCOPIC CHARACTERIZATION



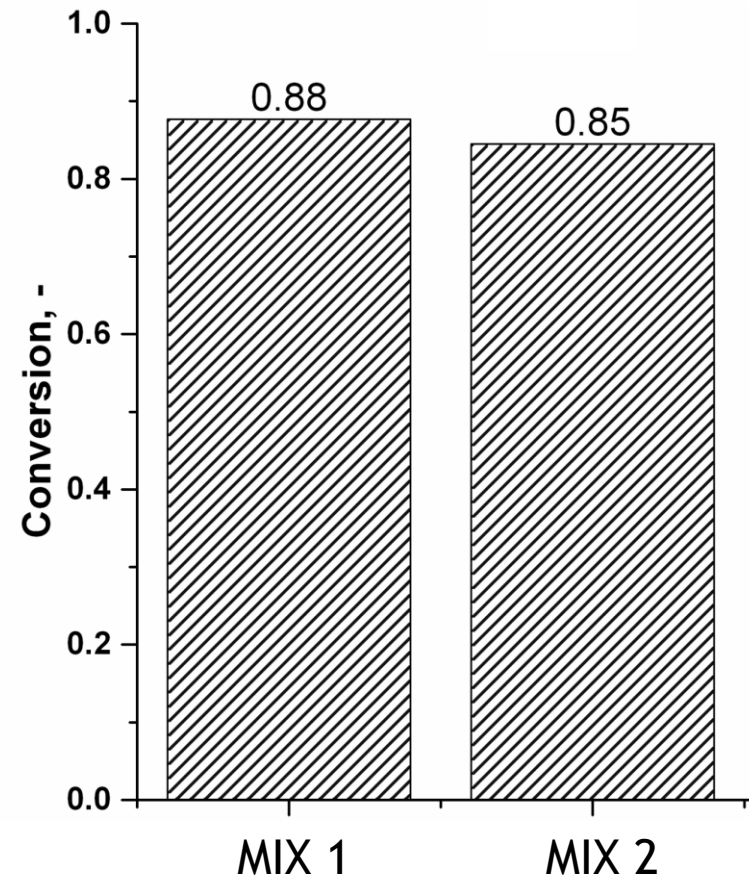
Raman spectrum for tested catalyst

# CATALYTIC ACTIVITY EVALUATION



Catalytic activity for tested catalyst for different flow conditions  
a) MIX 1, b) MIX 2

# CATALYTIC ACTIVITY EVALUATION



Conversion at 400°C for 6 dm<sup>3</sup>/min at different exhaust compositions

# CONCLUSIONS

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- ▶ Stainless steel wire mesh can be used as a support for CoPd/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalysts in methane combustion
- ▶ The T50% for the 1 dm<sup>3</sup>/min is achieved for ca. 250 °C, moves to the higher temperatures with the increasing of the gas exhaust flowrates. The almost complete conversion is achieved for all considered flowrates at 500 °C
- ▶ For more complex gas composition (composition II), the T50% moves towards the higher temperatures ca. 300 °C for flowrates 2 - 6 dm<sup>3</sup>/min. The conversion at 500 °C varies between 90% and 100%, with the lowest catalytic activity for the shortest residence time.

# REFERENCES

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# ACKNOWLEDGEMENTS

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This work was supported by:

- ▶ The National Centre for Research and Development (Project No. LIDER/204/L-6/14/ NCBR/2015)
- ▶ The Polish National Science Centre (Project No. 2015/17/D/ST8/01252)





# THANK YOU FOR YOUR TIME

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